Chem 466 Ceture# 21 04/08/2014 Thursday Exam I Quiz # 9 k = 6.1 5.0 = 3.7

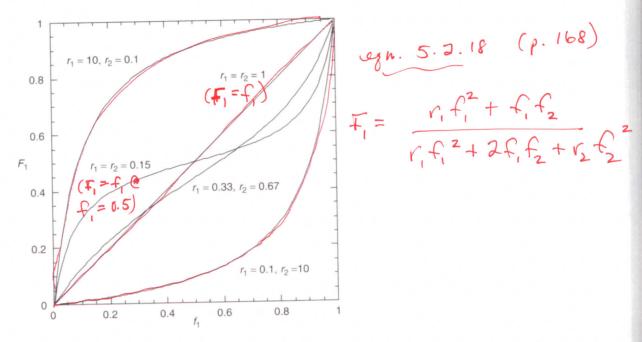


Figure 5.1 Mole fraction of component 1 in the copolymer as a function of feedstock composition for various reactivity ratios.

crossover point. At the crossover point the copolymer and feed mixture have the same composition. The monomer ratio at this point is conveniently solved by Equation 5.2.15:

$$\left(\frac{[\mathbf{M}_1]}{[\mathbf{M}_2]}\right)_{\text{cross}} = \frac{1-r_2}{1-r_1}$$
 (5.2.20)

For the case of $r_1 = 0.33$ and $r_2 = 0.67$ shown in Figure 5.1, $[M_1]/[M_2]$ equals 0.5 and $f_1 = 0.33$. This mathematical analysis shows that a comparable result is possible with both r_1 and r_2 greater than unity, but is not possible for $r_1 > 1$ and $r_2 < 1$.

6. When $r_1 = 1/r_2$, the copolymer composition curve will be either convex or concave when viewed from the F_1 axis, depending on whether r_1 is greater or less than unity. The further removed from unity r_1 is, the farther the composition curve will be displaced from the 45° line. This situation where $r_1r_2 = 1$ is called an *ideal copolymerization*. The example below explores the origin of this terminology.

There is a parallel between the composition of a copolymer produced from a certain feed and the composition of a vapor in equilibrium with a two-component liquid mixture. The following example illustrates this parallel when the liquid mixture is an ideal solution and the vapor is an ideal gas.

Example 5.1

An ideal gas obeys Dalton's law; that is, the total pressure is the sum of the partial pressures of the components. An ideal solution obeys Raoult's law; that is, the partial pressure of the *i*th component above a solution is equal to the mole fraction of that component in the solution times the vapor pressure of pure component *i*. Use these relationships to relate the mole fraction of component 1 in the equilibrium vapor to its mole fraction in a two-component solution and relate the result to the ideal case of the copolymer composition equation.

· Copolym equation defines ratio of monomer repeat units in poly vs. ratio of monomers in feed (rxn mixture) $\frac{d [m_1]/dt}{d [m_2]/dt} = \frac{[m_1]}{[m_2]} \left(\frac{r_1 [m_1] + [m_2]}{[m_1] + r_2 [m_2]} \right)$ ratio of monomer depends upon reachvity vatios repeat units in poly (i.e. consumed + monomer concentrations during polym) see Figure 5.1 (text p. 169) · when $r_1 \cong r_2 \cong 1 \Longrightarrow no pref. + random copolyon$ r, = r2 = 0 => no homopolym + alternating copoly r, >>1; r2=0=0 M, homopolym (r, >>1; r2 >0 =0 initially high M, polyn then M2 polyn if traditional us. controlled vadical polym. mixture of polys of a chain lengths + -> 000000 traditional: # A compositions M, O poly of similar controlled: 000000000000 chain lengths + > 0600000 06 ¢ 60 Deompositions along 00 500 80000 8 Ms o the ballisone

(I) practial polym. conditions

- 1. bulle polym
 - · no solvent
 - · cooling may be required, due to exothermicity of polym.
 - · shrinleage occurs
 - e monomer/polymen/initiator miscibilities are important
- 2. Solution polym.
 - · monomer/polymer/initiator solubilities
 que important
 - o dilution of solvent provides for heat transfer + smoother (more homogeneous) ran
 - · mw can be affected by conc.

3. Suspension polym.

- · storing required
 - · monomer droplets (10-1000 um diameter) Suspendel in H20
 - · initiator dissolved in monomer
 - · Suspending agents added

 H20 insoluble morganics, eg. barium sulfate

 if H20 soluble poly + H20 soluble mitator

 dispersion polym.



· polym proceeds like many individual bulk polym. (Same livetics)
gives large part les 10-1500 um
size + Dize dist dependent on Suspending agent + strong rate 4. Emulsion polym Sino final single singl · monomer dropteds (50nm-lum) suspended in H20 as ____ · mitiator (I) dissolved in Hed. · Surfactants (emils, Free) added - polym. occurs inside micelles

- diffusion controlled

- vate of diffusion of M + R. A PA 14to micelles Both wethods 3+4 can be used for most that insolible monomers The state out to lete.

particularly good for UF_=UF_2.

(J) Inhibitors + Retarders · used during storage of monomers to reduce polym. (unwanted) Inhibition constant, $Z = \frac{k_z}{k_p} = \frac{\text{rate constant for trapping}}{\text{rate constant for prop.}}$ Zx Rpolym. Rpolym L o species with high Z (>10) are inhibitors o species with low Z (<1) are retarders

retaile consumed retarder inhibitor (displaced curve) % con U. intrigitor consumed Time > induction period - no conversion (when all radicals are captured = D us polym.) prevents polym. as long as it is present (induction period, kz >10) · Inhibitor occurs so w/out inhibitor benzogninone

(Oatlade)

(Oatlade)

ether linkage these species

can undergo R-H + 0===0

exer further

w/ additional radicals

a quinone

(4 atom
als strack in)

Phenol (II) of it is a poorer whibitor R. (+ R-H R.) (1)-0-R BHT - used as a food antioxident (2,6-di-tert-butyl-4-methyl phenol) Peroxy radicals 2-3 peroxy radicals t-butyl catechol-is often used as inhibitor (e.s. when purchase styrene from Aldrich) H(I) OH R.

OH

O-H

R. + (+ R-H an o-quinone (which can undergo further radical scavenging)

a Retarder decreases the aut. of polym. by tropping some of the (Z<1) kprop > kz) - no induction period b/c no complete trapping of radicals - once retarder is consumed polymore occurs as w/out retarder P. VIII NO2 + R. (Catall) R. III NO2 R. 5 (Hatom abstraction) · retarder (not inhibitor) b/c reacts w/ radicals more slowly than kepiop R-(-)-NO2 + R-H · combo of monomer + additive detins whether inhibitor or retarder: [I] NO 2 e deficient Ar ring-reacts more reachly with e rich radicals

+ more reactive radicals

